

# Production of Syngas: Generation of Power and DME Synthesis

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## Abstract

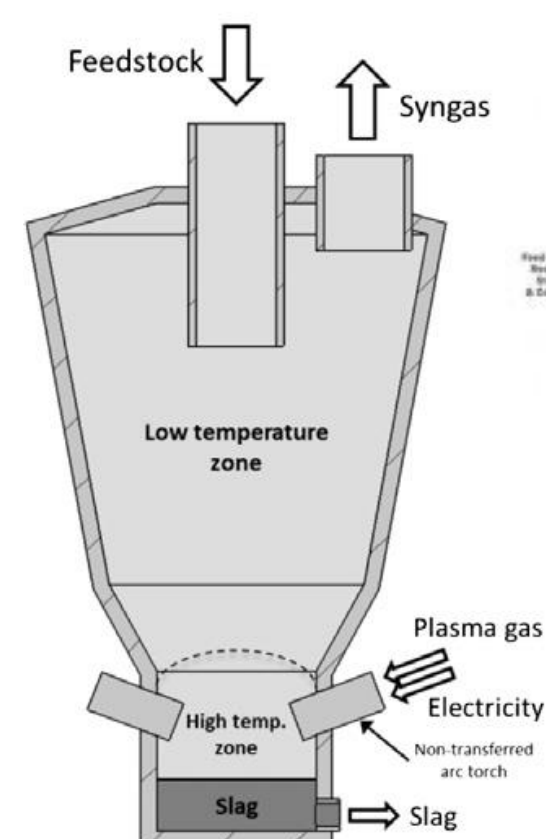
Refuse Derived Fuel (RDF) from municipal solid waste was used as the feedstock into a Plasma Gasifier in a two-step production process. Syngas, produced by the gasifier, was used as an energy source in a steam turbine that produced electricity. After losing heat, the syngas was then sent into a one-step synthesis process where it was converted into Methanol and Dimethyl Ether (DME) for sale. DME is used as an alternative to diesel fuel and Methanol is often used as a source for other products.

## Feedstock Composition and Analysis

Component	Weight Percent (%)
Paper	50.0
Sawdust	3.0
Wood	11.0
Vegetation	3.7
Cloth	5.5
Plastics	10.0
Rubber	3.5
Resins	1.0
Electronics	3.0
Debris	4.5
Glass	4.0

Component	Dry Basis Mole Fraction (%)
Carbon	50.5
Hydrogen	5.6
Oxygen	30.7
Nitrogen	1.1
Chlorine	<0.1
Sulfur	0.3

## Plasma Gasifier Diagram

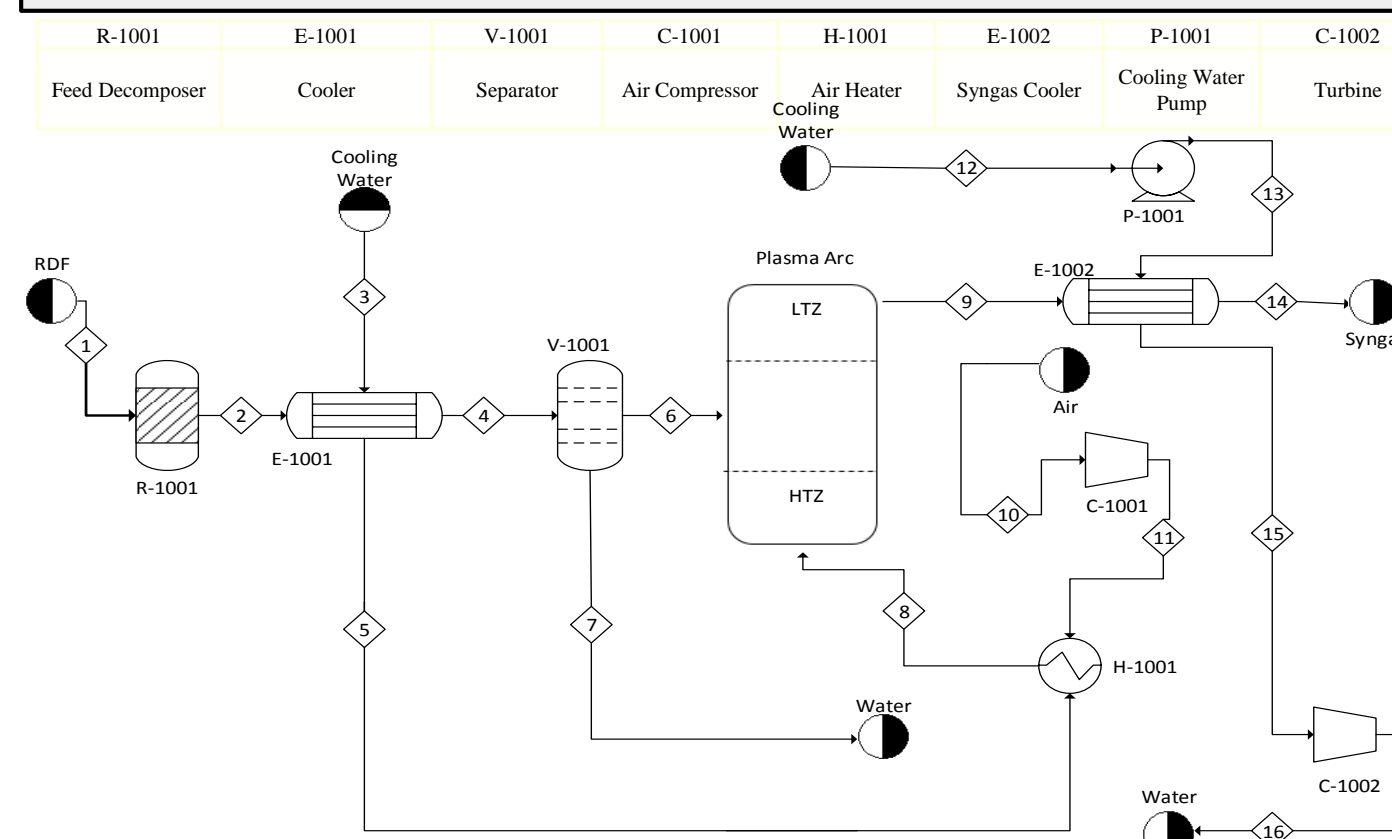


Source: [http://www.alternrg.com/waste\\_to\\_energy/](http://www.alternrg.com/waste_to_energy/)



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## 1. Plasma Gasifier



## Reactor Models

One-Step Synthesis Reactions:

[Bifunctional Catalyst]  $\text{CuO-ZnO-Al}_2\text{O}_3\cdot\gamma\text{-Al}_2\text{O}_3$



LHHW Kinetic Model (\* $K_1$ - $K_7$  Constants)

$$R_{\text{Hydrogenation}} = \frac{K_4 \left[ \frac{P_{\text{CO}_2} P_{\text{H}_2}}{1} - \frac{P_{\text{CH}_3\text{OH}} P_{\text{H}_2\text{O}}}{K_{E1} P_{\text{H}_2}^2} \right]}{\left[ 1 + K_3 \left( \frac{P_{\text{H}_2\text{O}}}{P_{\text{H}_2}} \right) + K_1 P_{\text{H}_2}^{0.5} + K_2 P_{\text{H}_2\text{O}} \right]^3}$$

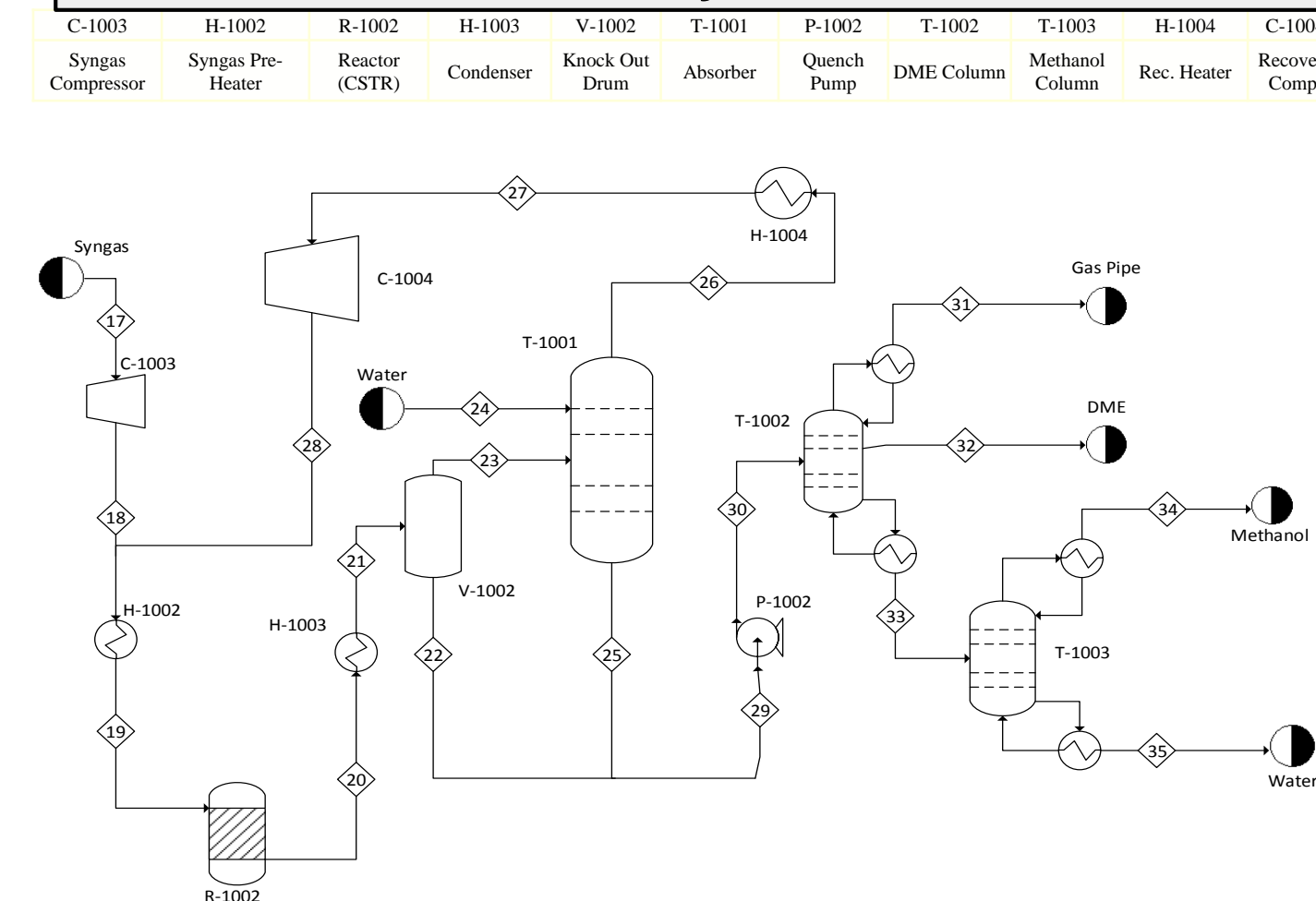
$$R_{\text{Dehydration}} = \frac{K_5 \left[ \frac{P_{\text{CO}_2}}{1} - \frac{P_{\text{CO}} P_{\text{H}_2\text{O}}}{K_{E2} P_{\text{H}_2}} \right]}{\left[ 1 + K_3 \left( \frac{P_{\text{H}_2\text{O}}}{P_{\text{H}_2}} \right) + K_1 P_{\text{H}_2}^{0.5} + K_2 P_{\text{H}_2\text{O}} \right]}$$

$$R_{\text{Water-Gas Shift}} = \frac{K_3 \left[ \frac{P_{\text{CH}_3\text{OH}}}{1} - \frac{P_{\text{DME}} P_{\text{H}_2\text{O}}}{K_3 P_{\text{CH}_3\text{OH}}} \right]}{\left[ 1 + K_7 P_{\text{CH}_3\text{OH}} + \frac{P_{\text{H}_2\text{O}}}{K_6} \right]}$$

## References

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## 2. DME Synthesis



## Stream Summary

Stream	Temp. (C)	Pressure (Bar)	Stream Cont.	Temp. (C)	Pressure (Bar)
1	25	1	17	270	30
2	300	1	19	250	50
6	80	1	20	260	50
8	4000	32	23	40	30.4
9	1600	1	31	184	30
14	250	1	32	199	33
15	1476	150	34	180	10
16	570	1	35	180	10

## Product Composition, Purity, and Power

Syngas (Mol Fraction)	
H <sub>2</sub> O	0.055
H <sub>2</sub>	0.517
CO	0.411
N <sub>2</sub>	0.005
S	0.001
CO <sub>2</sub>	0.011

Steam Turbine: Net Power	
6.1 MW	

Product	Purity
Methanol	99.7
DME	99.91

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